

#### **Effective CO<sub>2</sub>-capture technology development in Australia**

Paul Feron | Senior Principal Research Scientist

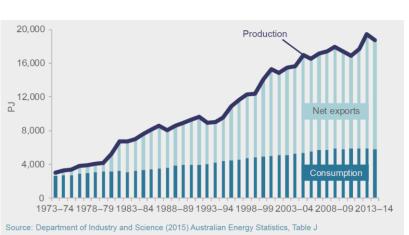
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CSIRO ENERGY www.csiro.au

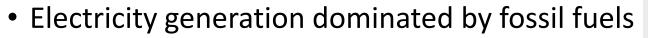


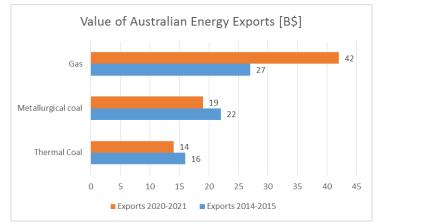
#### 2016 NETL CO<sub>2</sub> Capture Technology Project Review Meeting

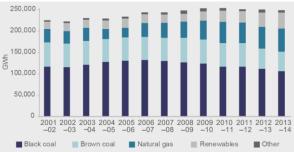
## **CCS drivers in Australia**



• Export of fossil fuel products







Source: Department of Industry and Science (2015) Australian Energy Statistics, Table

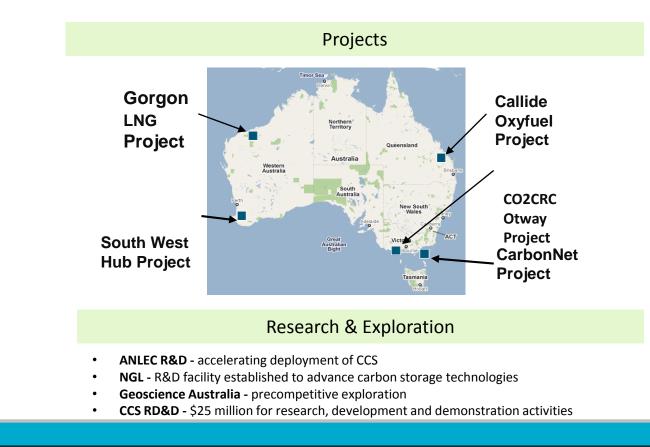


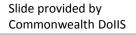
## **Australia's approach to CCS**

- Policy position
- Understanding the CCS resource
- Demonstrating domestic LET capacities & capabilities
- Strategic partnering
- Building Australian skills and capacity
  Innovation



#### The Story So Far in Australia Key CCS Projects & Key Research Initiatives





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## Australian coal fired power stations

			(150
	Black coal	Brown coal	australia
Average efficiency [% HHV]	35.6	25.7	Australia Fuel 50 0 Cap
CO <sub>2</sub> emission [tonne/MWh]	0.9	1.3	
SO <sub>2</sub> concentration [g/m <sup>3</sup> ]	0.5 – 1.7	0.2 - 0.7	No CO <sub>2</sub> Capture 90 % CO <sub>2</sub> Capture
NO <sub>x</sub> concentration [g/m <sup>3</sup> ]	0.4 – 1.5	0.2 - 0.4	PCC Investment costs 8% 27% 9 FGD + SCR 9 Pre-treatment 9 Blower 9 Absorber 9 Heat exchangers 9 Stripper/Reboiler 0% 14%
Particulate matter [mg/m³]	10 - 100	10 - 60	
Flue gas temperature [°C]	120	180	
Data derived from	n CCSD – technology assessm	nent report 62	



# **PCC technology requirements**

# Energy Efficient

• Towards zero energy penalty

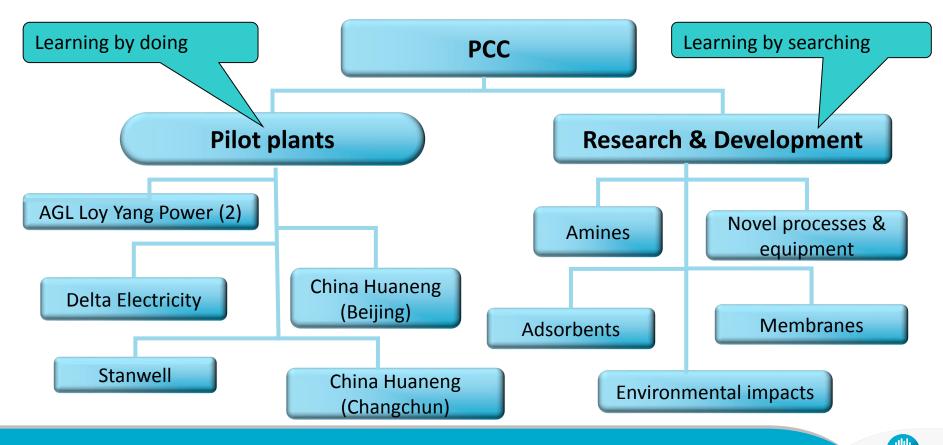
## > Affordable

• Costs lower than other LET's

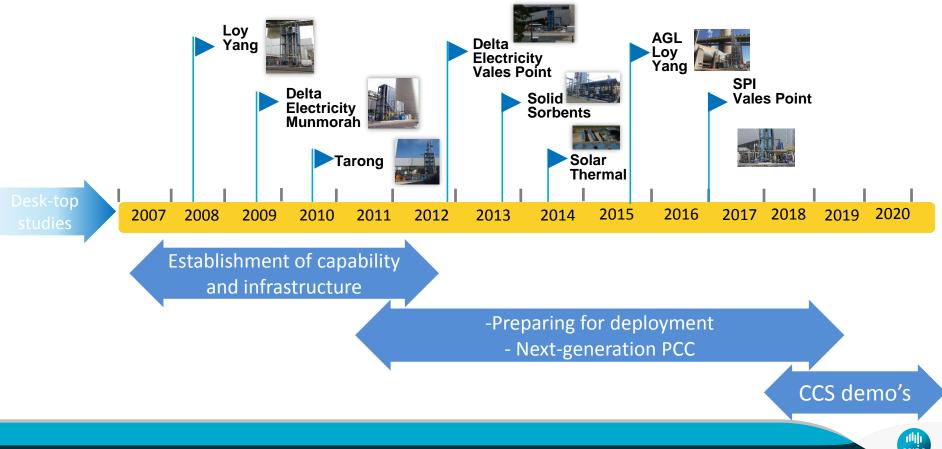
## Environmentally benign

• Zero harm to the environment

## **CSIRO's PCC program**



### **Piloting PCC Technologies in Australia**



# **PICA Project**

#### **Project aims:**

40% lower cost of CO<sub>2</sub> capture compared to the MEA base case

□ Advanced packing materials, liquid absorbent and process

- to provide information on long-term performance and reliability of advanced liquid absorbents and equipment that have been developed in-house by both IHI Corporation and CSIRO independently in preparation of demonstration phase
- Supporting large-scale CCS as an affordable, secure and environmentally benign option for power generation

http://www.csiro.au/en/News/News-releases/2016/PICA-powers-up-to-improve-CO2-capture







# **Approaches for reduction capture energy**

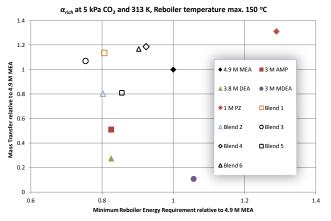
- Development of amine formulations/new amines
- Process development
  - Novel process design
  - □ Innovative equipment
- Renewable energy integration
  - Solar thermal
  - □ Light swing absorbents
- Integration with Direct Carbon Injection Engine
- Absorption enthalpy conversion

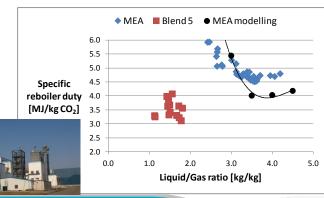


## **Development of amine formulations/new amines**

#### Formulations base on primary amines

- □ Selection of a first amine that reacts rapidly with CO<sub>2</sub> through the formation of a carbamate
- □ Selection of a second amine:
- preferably with little or no carbamate formation and being a stronger base than the first amine
- such that the enthalpy of protonation is large to maximise the temperature dependent pH change to aid thermal desorption of CO<sub>2</sub>
- Optimisation of the formulation composition to achieve acceptable physical properties
- $\Box$  Assessment of CO<sub>2</sub> absorption rates and reboiler duties
- Designer amines and functionalised amines
  Focus on diamines with dual functionality
  Higher molecular efficiency

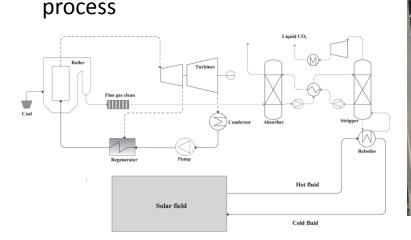






## Solar thermal energy for absorbent regeneration

- Avoiding interface with existing steam cycle
- More effective in terms of CO<sub>2</sub>-emission reduction
- Introduction of flexibility into the capture



Pilot plant at Vales Point power station

- Integrated with existing PCC pilot plan
- 65 kW<sub>th</sub> solar array



http://arena.gov.au/files/2015/08/3-A006-Final-Report-and-Lessons-Learnt.pdf



# **Approaches for reduction capital costs**

- Development of amine formulations/new amines
- > Aqueous ammonia process development
- Packingless contactors: the rotating liquid sheet contactor
- ➢ Integrated removal of SO₂ and CO₂: CS-CAP
- Selective flue gas recirculation
- Solid sorbents
- Membrane assisted liquid absorbent regeneration



### **Rotating Liquid Sheet contactor**

### **Basic principles**

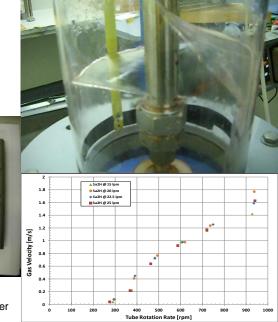
- Surface area of stabilized liquid sheet greater than that of resulting droplets.
- Rotating liquid surface proven experimentally to pump gas.
- Centrifugal + liquid pumping force creates interfacial area.

### Advantages

- Higher gas velocities possible.
- Liquid entrainment significantly reduced
- Suitable for viscous solvents

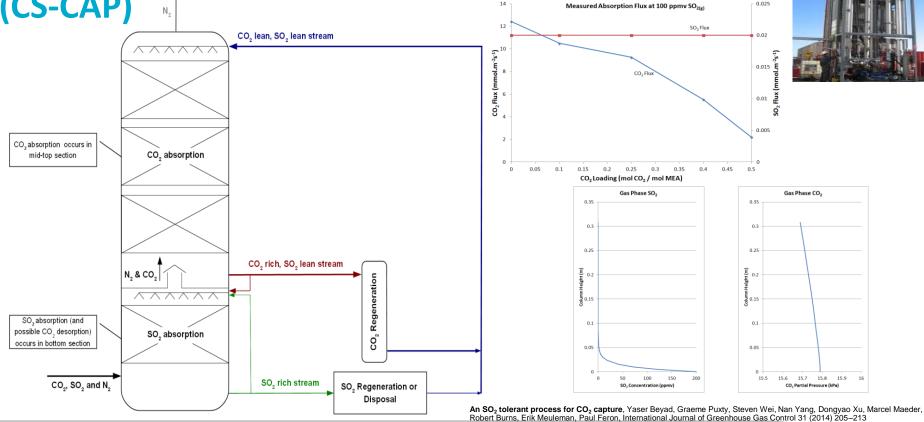
### Challenges

- Scale-up to commercial scale
- Liquid residence time low





### Integrated Single Stream SO<sub>2</sub> and CO<sub>2</sub> Capture (CS-CAP) N<sub>2</sub> Measured Absorption Flux at 100 ppm SO<sub>2160</sub>

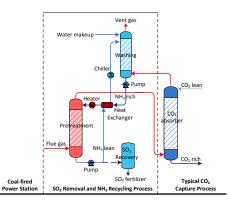




### **Aqueous ammonia for PCC in Australia**

- Indestructable liquid absorbent
- Chemical well-known to electricity industry
- Suited for "contaminated" feed gases
- Fertiliser by-product
- Product CO<sub>2</sub> at elevated pressure
- Technical feasibility demonstrated in pilot plant but no cost advantage
- Addressing challenges:
  - □ Mass transfer promotion, temperature increase
  - □ Vapour suppressors
  - □ Further integration of pretreatment and water wash
  - Process design





#### Li et al., Environ. Sci. Technol. 2015, 49, 10243-10252

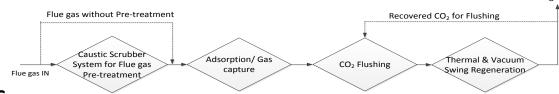


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### Solid sorbent CO<sub>2</sub> Capture Unit at Vales Point power station

#### > Objective

- □ to evaluate the stability of honeycomb CF composite monolithic adsorbents using the real flue gas at Vales Point Power Station
- □ to understand the effect of real flue gas characteristics on the operation and performance of the CO<sub>2</sub> capture unit

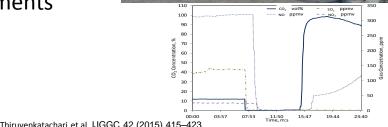


#### ➢ Results

- □ Excellent stability to real flue gas over 200 experiments
- $\Box$  CO<sub>2</sub> adsorption efficiency consistently over 98%
- $\Box$  CO<sub>2</sub> desorption efficiency between 90-95%
- $\Box$  Near complete removal of SO<sub>2</sub> and NO<sub>x</sub>
  - Could be pretreatment unit for amine based PCC Thiruvent







### Emission issues addressed via integrated risk-based approach

Formation of potentially harmful components
 Absorbent degradation in absorber
 Absorbent degradation in desorber

#### 2. Emission analysis

Estimation of concentrations using process models
 Actual measurements in pilot plants

#### 3. Dispersion

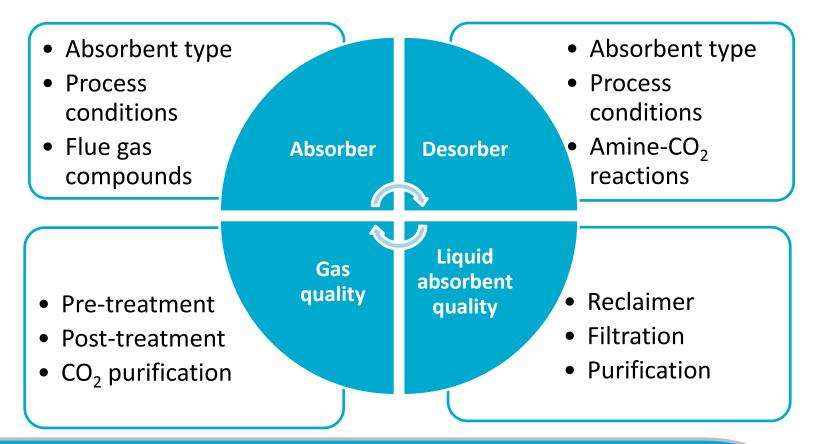
Environmental chamber to investigate atmospheric degradation
 Updating dispersion models with atmospheric chemistry







#### Managing environmental impacts of amine based PCC processes





### **Outlook for PCC in Australia – Next steps**

- Qualification of new liquid absorbents towards deployment
  Formulations and designer amines
  Optimisation of process design
- > Development of  $SO_2/CO_2$  process concepts
- Focus on process & equipment innovation
- Solar thermal integration demonstration
- - Advanced liquid absorbent systems

### Acknowledgements



# Thank you

#### Energy

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**CSIRO TV** <u>http://tv.csiro.au/#v=xbz189hynwj6</u>





### **Reference materials**

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- Research Opportunities in Post Combustion CO<sub>2</sub> Capture, Paul H.M. Feron et al., October 2009, available from <u>www.anlecrd.com</u>
- Assessing Atmospheric Emissions from Amine-based CO<sub>2</sub> Post-combustion Capture Processes and their Impacts on the Environment – A Case Study: Volume 1 - Measurement of emissions from a monoethanolamine-based post-combustion CO2 capture pilot plant, Merched Azzi et al., report to Global Carbon Capture and Storage Institute, May 2014
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